

Ignition of hydrogen-air mixtures under volumetric expansion

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7th International Conference on Hydrogen Safety - Hamburg, GER

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Monday September 11, 2017



outlines

- 1 Introduction
- 2 Methodology and calculation procedure
- 3 Results and discussion
- 4 Conclusion

Formation of expansion waves

SW-obstacle



SW diffraction



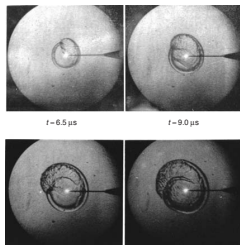
Expansions can be formed in complex pipelines
Important for shock ignition and industrial safety

Simulations by Prof. H. Hornung

Re-initiation behind a decaying shock wave (1)

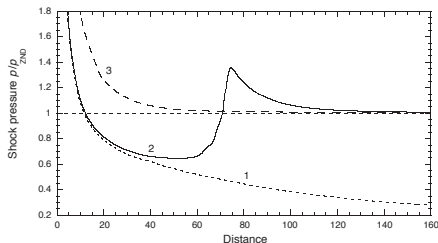
Detonation direct initiation

2-D images



Bach et al., 1969

1-D simulations



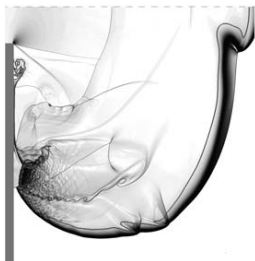
Ng and Lee, 2003

SW velocity decreases much below D_{CJ} before re-initiation occurs

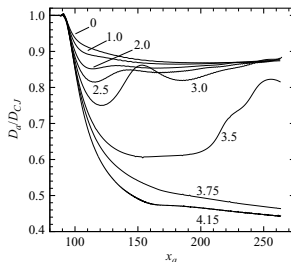
Re-initiation behind a decaying shock wave (2)

Detonation diffraction

2-D simulations



Velocity along the axis



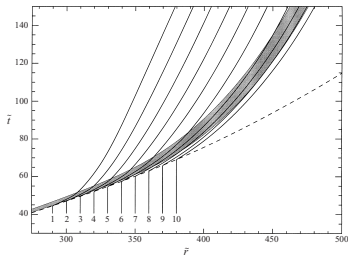
SW velocity decreases much below D_{CJ} before re-initiation occurs

Results from Arienti and Shepherd, 2005

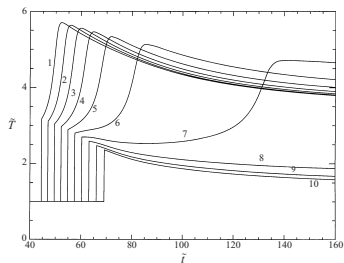
Reaction in expanding flows (1)

Lagrangian particles

Particle path



Temperature profile



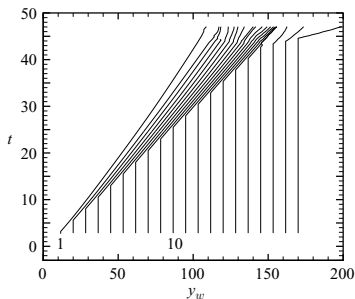
As the SW decays, ignition delay-time increases and the reaction is eventually quenched

Results from Eckett et al., 2000

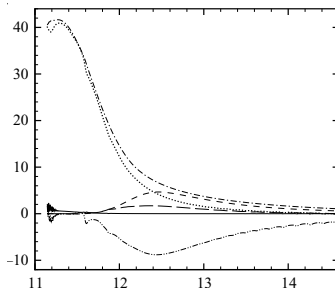
Reaction in expanding flows (2)

Ignition dynamics

Particle path



Energy equation analysis

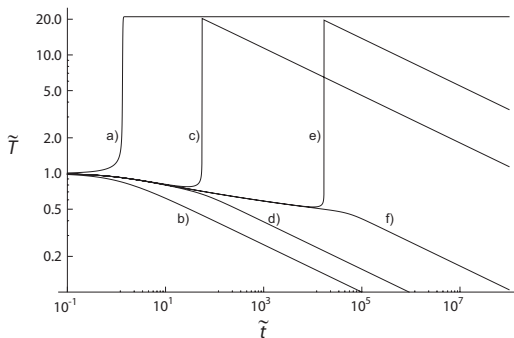


Chemical energy release vs unsteadiness

Results from Arienti and Shepherd, 2005

Previous work on reacting expanding flows

Lundstrom and Oppenheim, Eckett et al., Arienti and Shepherd, Radulescu and Maxwell



1-step chemical models were used

Purpose of the study

Investigate the effect of volumetric expansion on the chemical kinetics of hydrogen-air mixtures

Approach

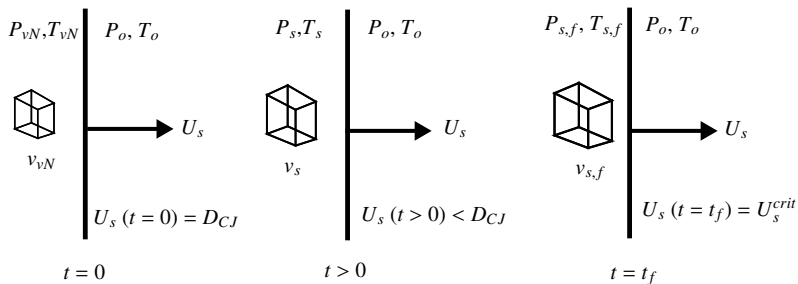
- **Chemistry : detailed reaction model**
- **Flow : simple reactor model to describe expansion**
- **Scope : perform detailed kinetics analyses**

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Problem definition

Specific volume behind a decaying SW



Gas expands behind SW as time progresses
Chemical reactions do not take place at constant pressure or volume...
cooling needs to be considered

Mathematical formulation ⁽¹⁾

Three forms for the rate of SW velocity decrease

- **Linear** : $U_S(t) = D_{CJ} - \alpha t$
- **Exponential** : $U_S(t) = D_{CJ} \exp(-\beta t)$
- **Power law** : $U_S(t^*) = D_{CJ} (t^*)^{-\delta}$

α , β , and δ are adjusted so that $\Delta T / \tau$ through isentropic expansion is the same

- **Linear** : $\alpha(\Delta T) = D_{CJ} - U_S(\Delta T)$
- **Exponential** : $\beta(\Delta T) = \ln(D_{CJ} / U_S(\Delta T))$
- **Power law** : $\delta(\Delta T) = \frac{\ln(D_{CJ} / U_S(\Delta T))}{\ln(2)}$

Mathematical formulation (2)

Final time of simulation

- **Linear** : $t_{f,Lin} = \frac{D_{CJ} - U_S^{crit}}{\alpha(\Delta T)}$
- **Exponential** : $t_{f,Exp} = \frac{\ln(D_{CJ}/U_S^{crit})}{\beta(\Delta T)}$
- **Power law** : $t_{f,PW}^* = \left(\frac{D_{CJ}}{U_S^{crit}} \right)^{1/\delta(\Delta T)}$

When SW becomes an acoustic wave ($M \sim 1$)

Calculation procedure

Numerical routine including the following steps

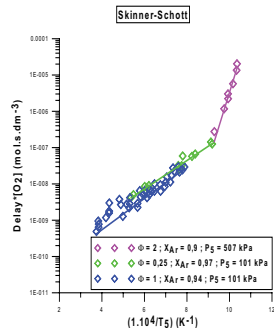
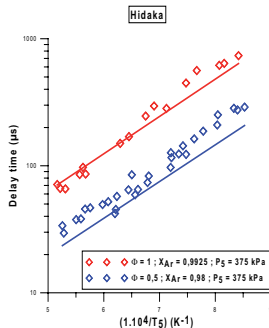
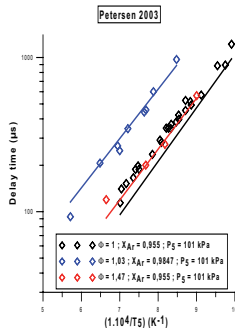
- Calculate D_{CJ}
- Calculate P_{vN} and T_{vN} for $U_S = D_{CJ}$
- Calculate τ_{Th} at P_{vN} and T_{vN} using a CP reactor
- Calculate $P_S(\Delta T)$ using the isentropic relationship for a given ΔT
- Calculate the corresponding $U_S(\Delta T)$
- Calculate the shock decay rates coefficients : α , β and δ
- Calculate t_f (or t_f^*) for all decay rates
- Construct time vector in the range $[0, t_f]$
- Calculate shock velocity, U_S , corresponding to each element of the time vector
- Calculate $P_S(t)$ corresponding to each value of $U_S(t)$
- Calculate specific volume, v , starting from P_{vN} and T_{vN} , and considering an isentropic expansion
- Calculate τ_{Th} with the volume vs. time option (VTIM)

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Reaction model validation (1)

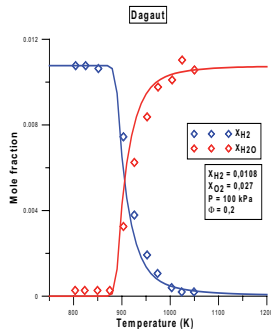
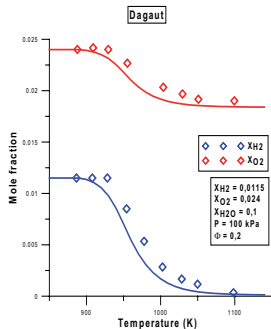
Shock tube data



Good agreement

Reaction model validation (2)

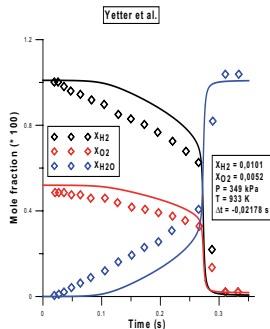
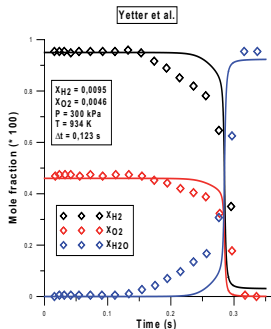
Jet-stirred reactor data



Good agreement

Reaction model validation (3)

Flow reactor data

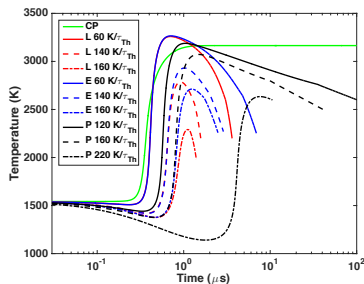


Reasonable agreement

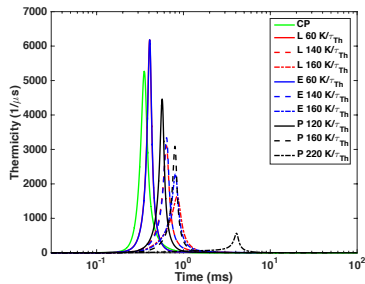
Effect of expansion on the ignition dynamics

Cooling rate 0-250 K/ τ

Temperature profiles



Thermicity profiles

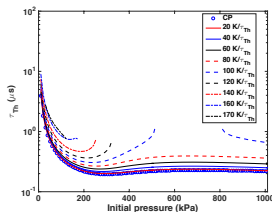


**As cooling rate is increased
 τ increases and σ_{max} decreases**

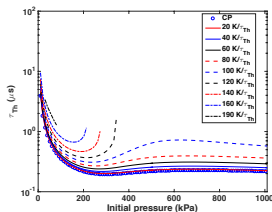
Effect of expansion on τ

$P_1 = 10\text{-}1000$ kPa and Cooling rate $0\text{-}250$ K/ τ

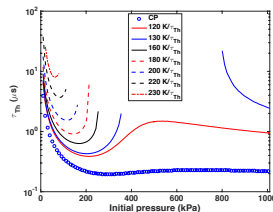
Linear decay



Exponential decay



Power law decay



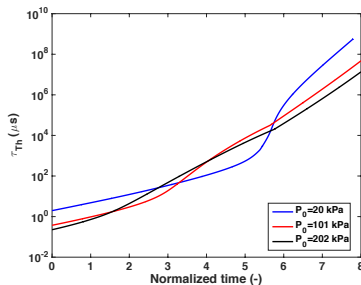
Highest sensitivity to quenching for $P_1 = 500\text{-}800$ kPa
Lowest sensitivity to quenching for $P_1 < 100$ kPa

Variation of CP τ along isentropes

Effect of initial pressure

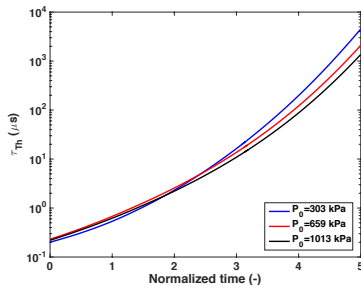
Low pressure range

(Exponential decay)



High pressure range

(Linear decay)



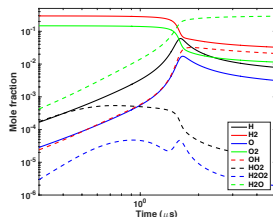
At LP, 2nd explosion limit is located at lower T

At HP, delay-time decreases as P increases

Species profiles

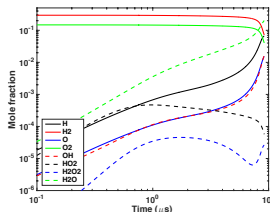
Power law decay rate

Sub-critical



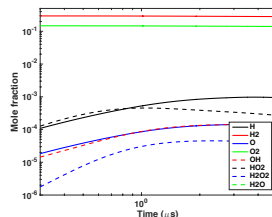
200 K/ τ

Near-critical



225 K/ τ

Super-critical



230 K/ τ

At 225 K/ τ , runaway just before final time

At 230 K/ τ , no significant consumption of reactants

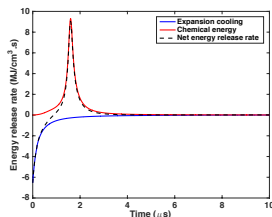
Energy release

Chemical energy vs Cooling (expansion)

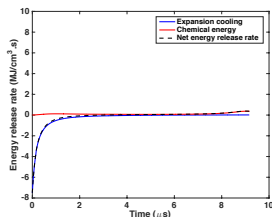
Sub-critical

Near-critical

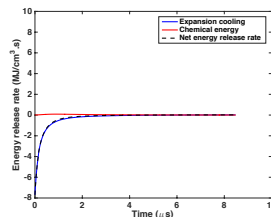
Super-critical



$200 \text{ K}/\tau$



$225 \text{ K}/\tau$



$230 \text{ K}/\tau$

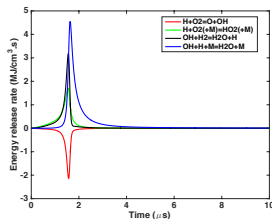
At $225 \text{ K}/\tau$, weak energy release at longer time

At $230 \text{ K}/\tau$, no significant energy release

Energy release per reaction

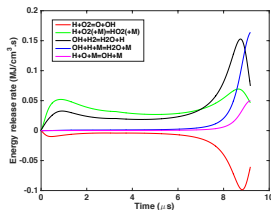
Focus on chemical energy release

Sub-critical



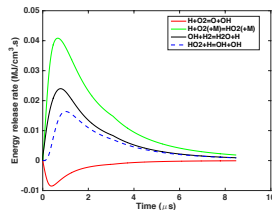
200 K/τ

Near-critical



225 K/τ

Super-critical



230 K/τ

At ≤ 225 K/τ :

Induction : $\text{H} + \text{O}_2(+\text{M}) = \text{HO}_2(+\text{M})$

Exothermic : $\text{OH} + \text{H}_2 = \text{H}_2\text{O} + \text{H}$ and $\text{OH} + \text{H}(+\text{M}) = \text{H}_2\text{O}(+\text{M})$

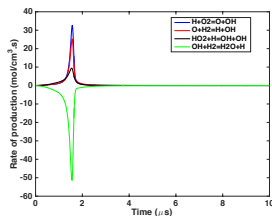
At > 225 K/τ :

No switch to branching chemistry

Rate of production

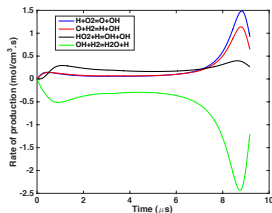
Analysis for OH radical

Sub-critical



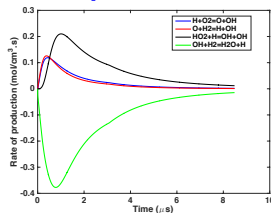
200 K/τ

Near-critical



225 K/τ

Super-critical



230 K/τ

At \leq 225 K/τ :

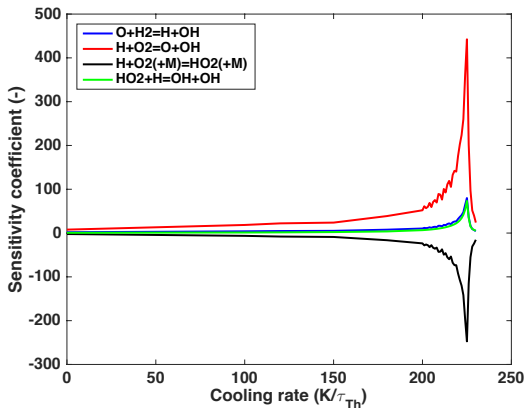
Double inversion between linear chain and chain branching

At $>$ 225 K/τ :

Single inversion between linear chain and chain branching

Sensitivity coefficient on OH

Evolution as a function of cooling rate



Increasing sensitivity and competition between linear chain and chain branching

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Conclusion

Study of chemical kinetics of hydrogen-air mixtures under volumetric expansion

- Power law decay is the least efficient at quenching the reaction
- Intermediate pressure ($P_1 = 500\text{-}800\text{ kPa}$) are the most sensitive to quenching
- Low pressure ($P_1 < 100\text{ kPa}$) are the least sensitive to quenching
- Complex response to expansion is due to the extended second explosion limit

Acknowledgments

Thank you for your attention

Questions ?

