



IA HySafe Research Priorities Workshop on Hydrogen Safety  
26-27 September 2016, Petten, the Netherlands

# **Research progress, near term research directions, and gaps of knowledge**

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# Acknowledgements

## HySAFER team

- ❖ Dr Sile Brennan
- ❖ Dr Volodymyr Shentsov
- ❖ Dr James Keenan
- ❖ Dr Sergii Kashkarov
- ❖ Dr Yangkyun Kim
- ❖ Dr Wookyung Kim

## Research projects

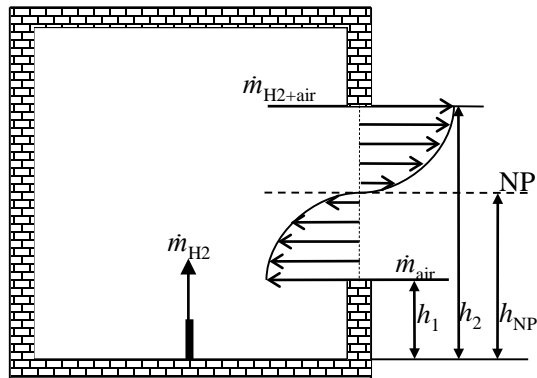
- ❖ EC H2FC Research Infrastructure
- ❖ FCH-JU HyIndoor
- ❖ FCH-JU HyResponse
- ❖ UK EPSRC H2FC SUPERGEN Hub
- ❖ UK EPSRC H2FC SUPERGEN Challenge

# Progress : releases

## Natural vs passive ventilation for single vent

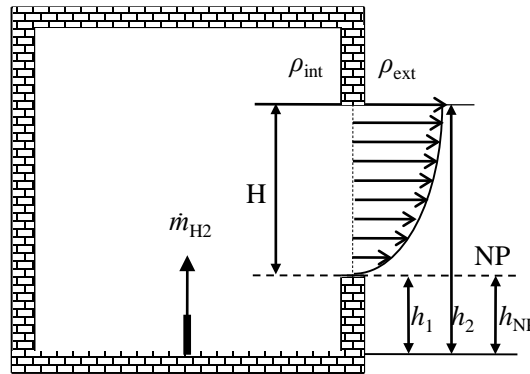
### Fixed neutral plane

$$X = \left[ \frac{Q_0}{C_D A (g' H)^{1/2}} \right]^{2/3}$$

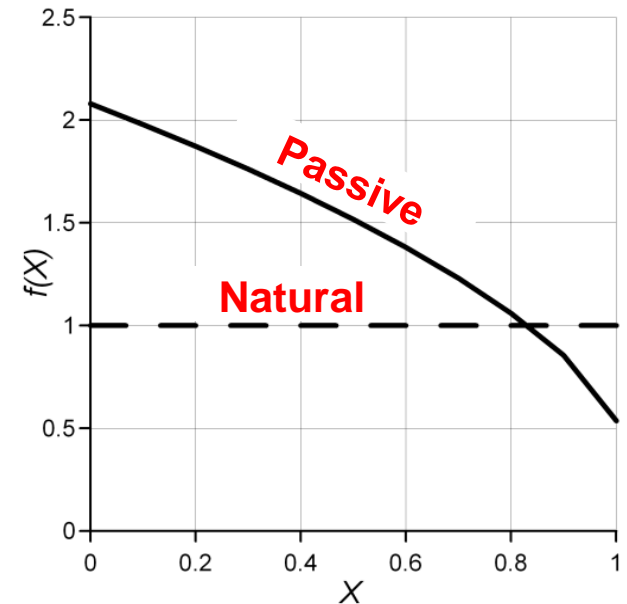


### Variable neutral plane

$$X = f(X) \cdot \left[ \frac{Q_0}{C_D A (g' H)^{1/2}} \right]^{2/3}$$



Difference: 
$$f(X) = \left( \frac{9}{8} \right)^{1/3} \cdot \left\{ \left[ 1 - X \left( 1 - \frac{\rho_{H_2}}{\rho_{air}} \right) \right]^{1/3} + (1 - X)^{2/3} \right\}$$



### Natural ventilation

- ❖ Underestimate **x2 (lean)**
- ❖ Overestimate **x2 (rich)**

### Example

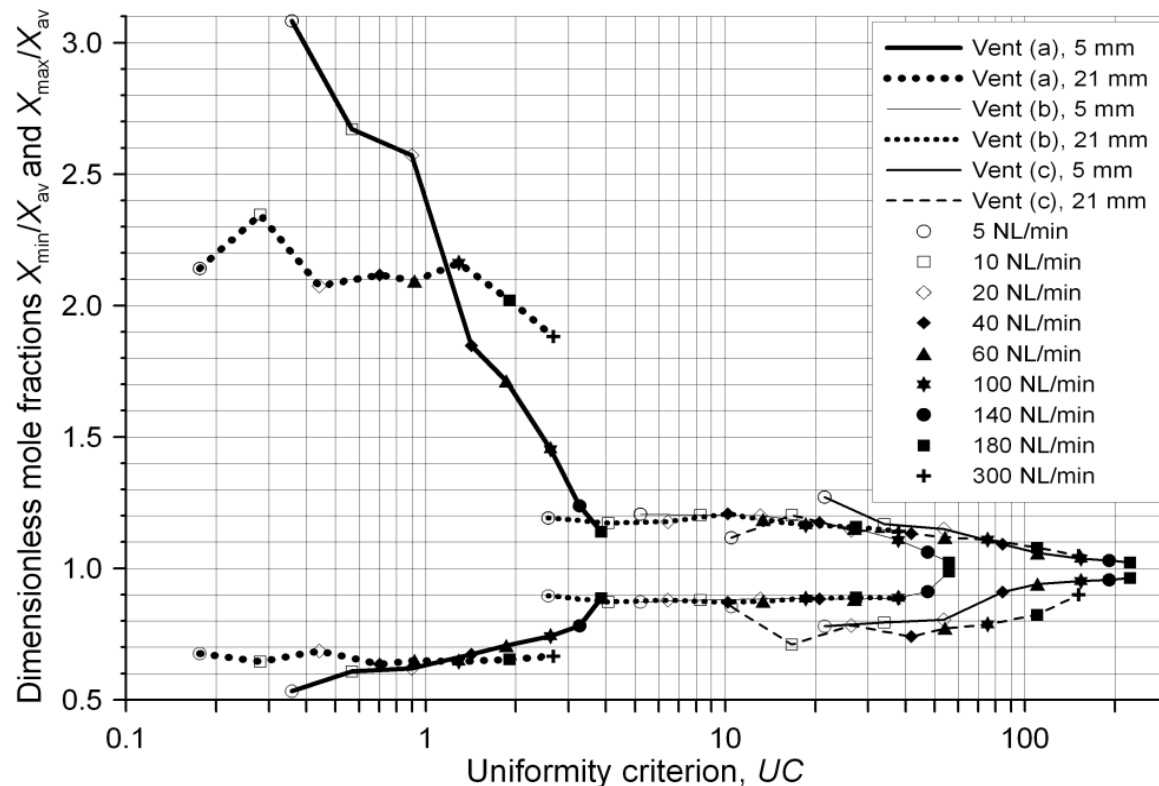
- ❖ Natural 3.5% v/v < LFL
- ❖ Passive > 7% v/v > LFL

# Progress: releases

## Passive ventilation for single vent

### Criterion for uniformity

$$UC = \frac{V^{2/3} \sqrt{D}}{A \sqrt{H}} \frac{\dot{m}_{ent}(x)}{\dot{m}_{mix}} \quad \dot{m}_{ent}(x) = K_1 M_0^{1/2} \rho_{mix}^{1/2} x$$
$$\dot{m}_{mix} = \dot{m}_{H_2} + \dot{m}_{air}$$

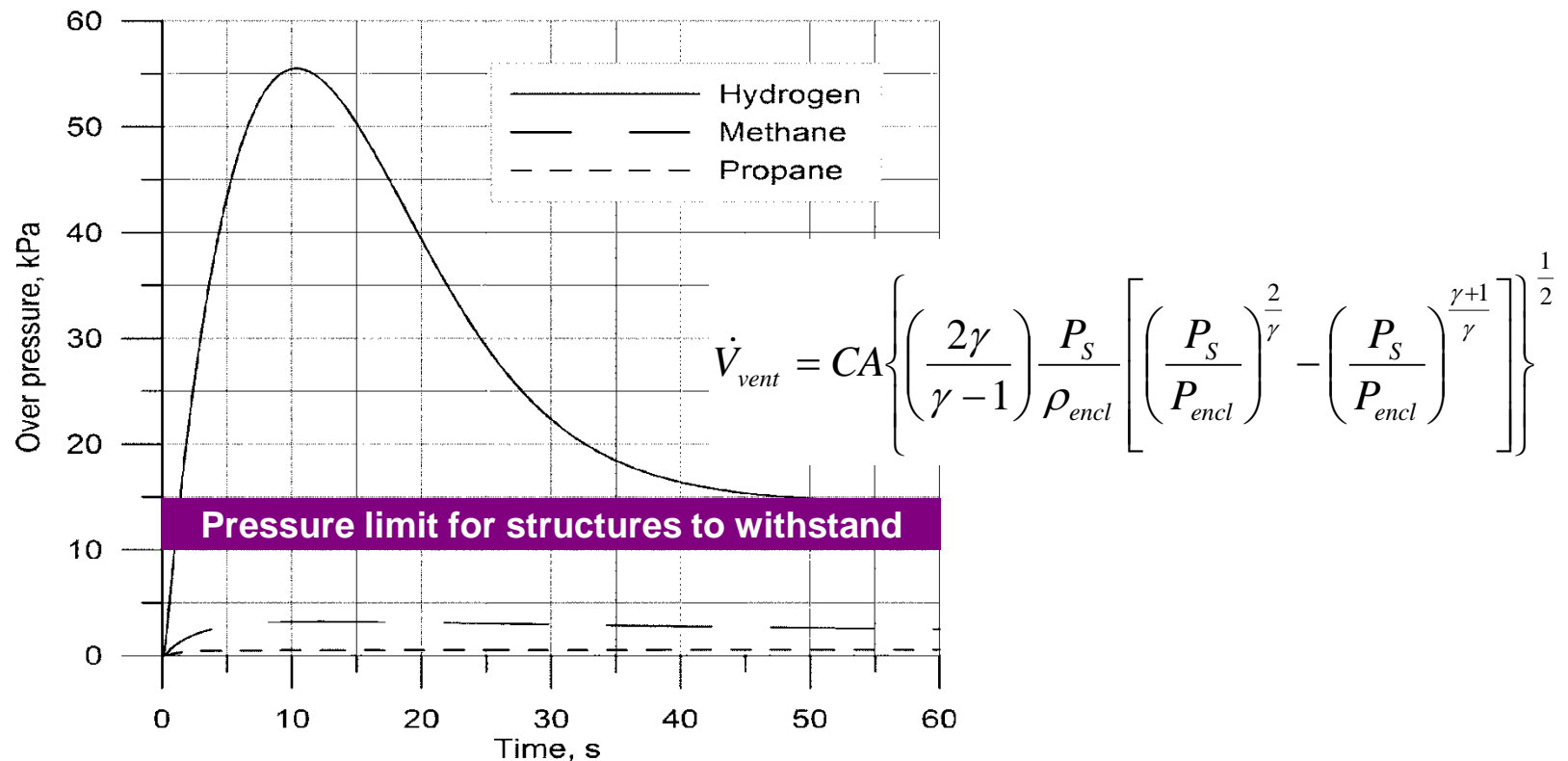


# Progress : releases

## PPP for non-reacting release

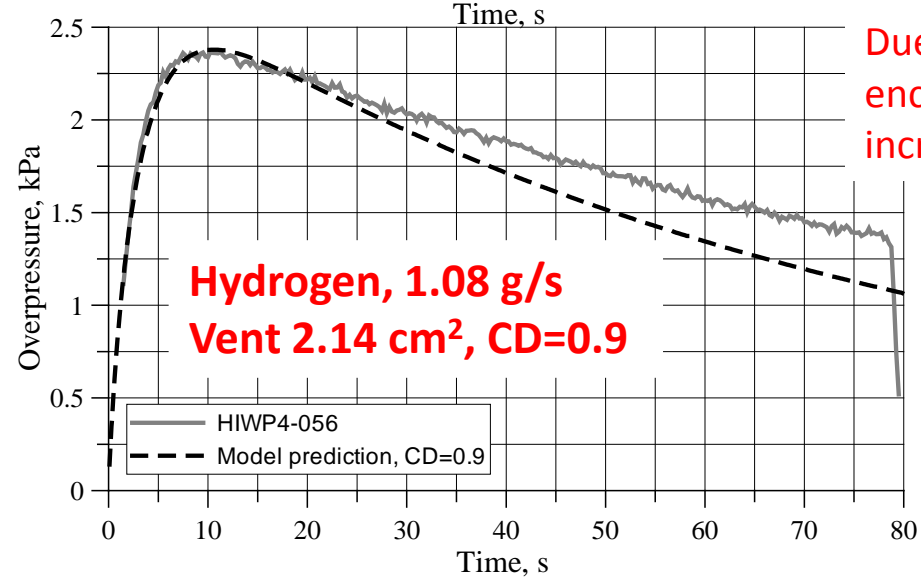
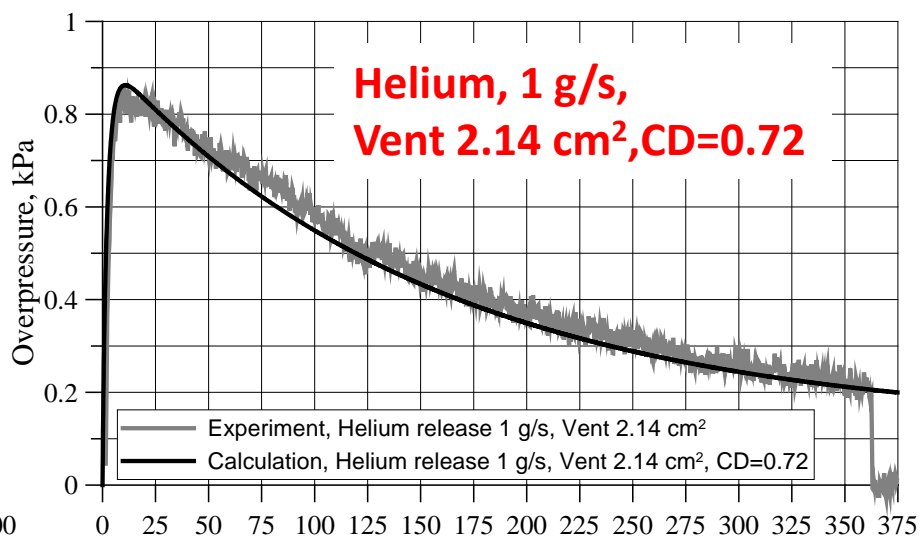
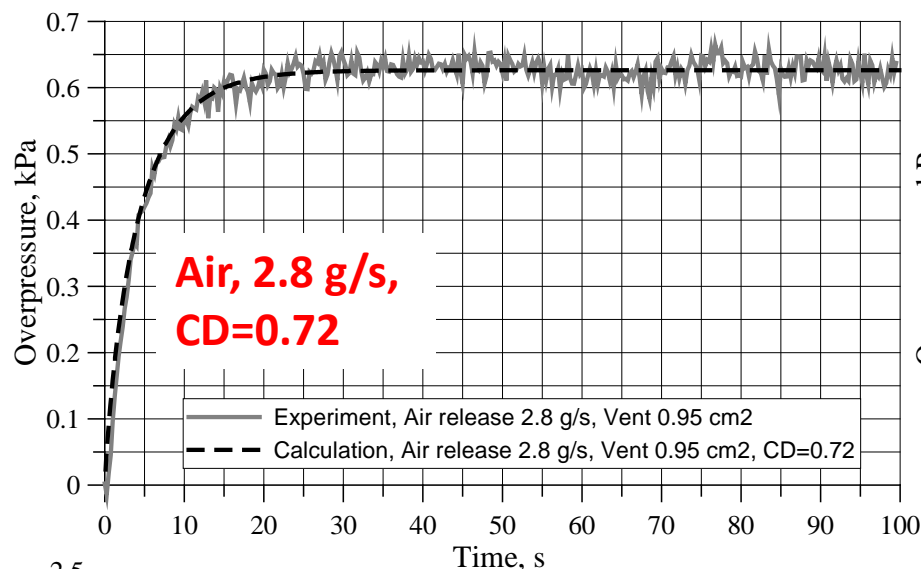
Example of pressure peaking phenomenon (PPP) for non-reacting release:

- ❖ Garage  $L \times W \times H = 4.5 \times 2.6 \times 2.6$  m, “brick” vent
- ❖ CGH2 storage: 350 bar,  $\varnothing 5.08$  mm orifice, mass flow rate 390 g/s

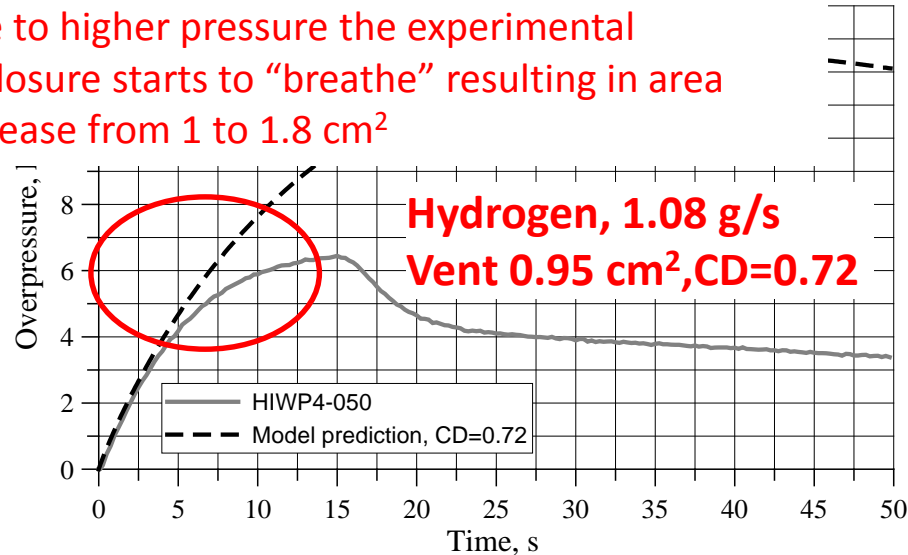


# Progress: releases

## Validation of PPP model, non-reacting release



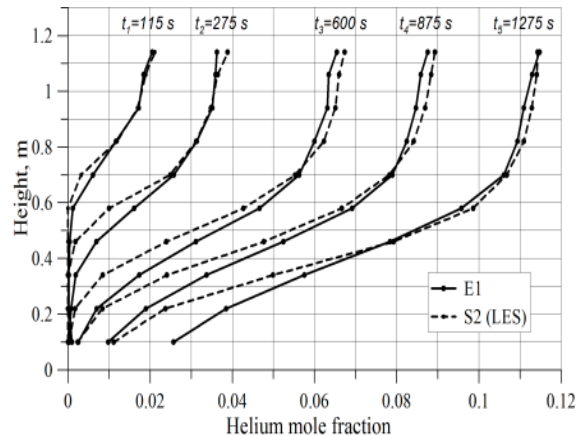
Due to higher pressure the experimental enclosure starts to “breathe” resulting in area increase from 1 to 1.8 cm<sup>2</sup>



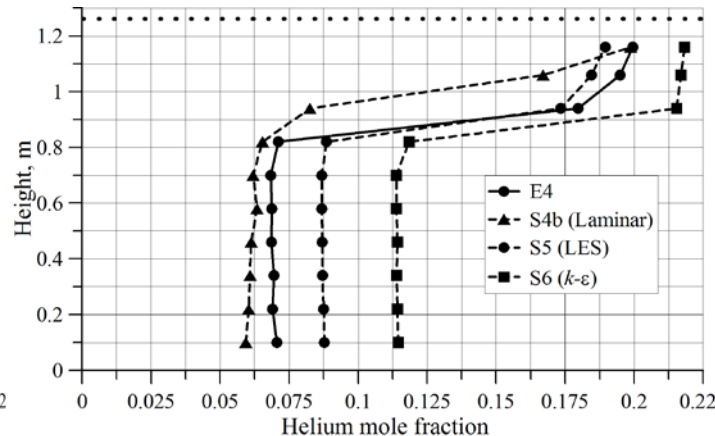
# Progress: releases

## LES of indoor releases

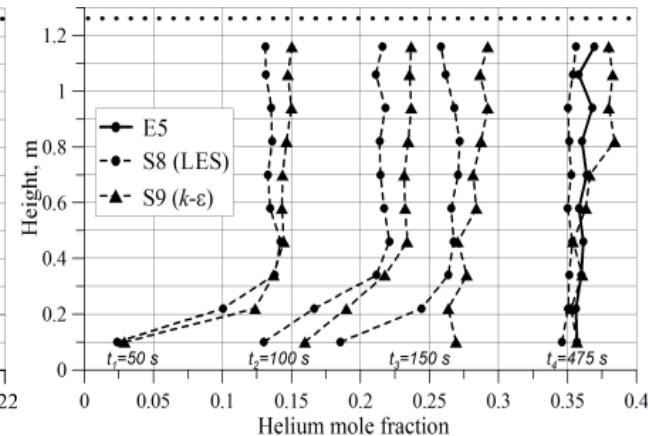
Laminar release  
 $Re=39$



Transitional release  
 $Re=2863$



Turbulent release  
 $Re=6968$



Experiment: Cariteau B., Tkatschenko I., *Int.J.Hydrog.Energy*, vol. 38, pp. 8030–8038, 2013

**LES performs best though range of release regimes (laminar to weakly turbulent)**

- ❖ Laminar
  - LES reproduces laminar release and dispersion (when properly applied)
- ❖ Transitional
  - LES outperforms standard  $k-\epsilon$  model
- ❖ Turbulent
  - LES and  $k-\epsilon$  models reproduce weakly turbulent flow
  - laminar model - not applicable

# Progress: jet fires

## Regimes of indoor jet fires

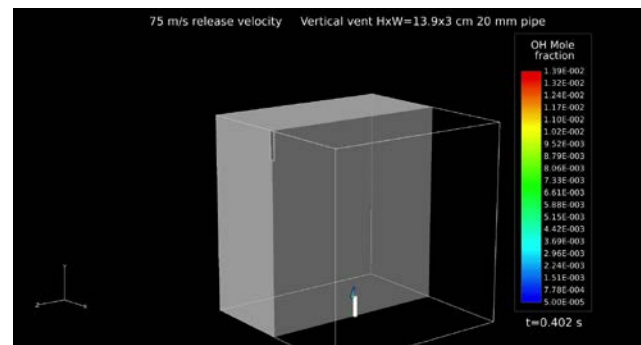
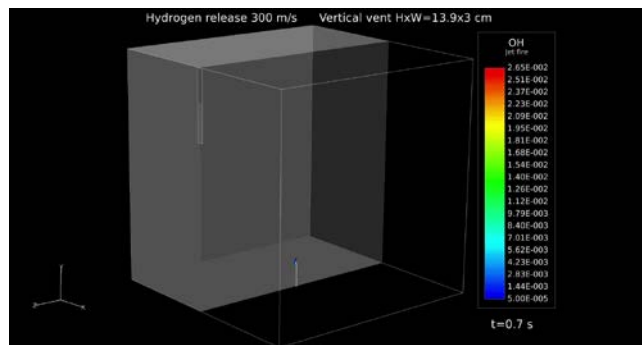
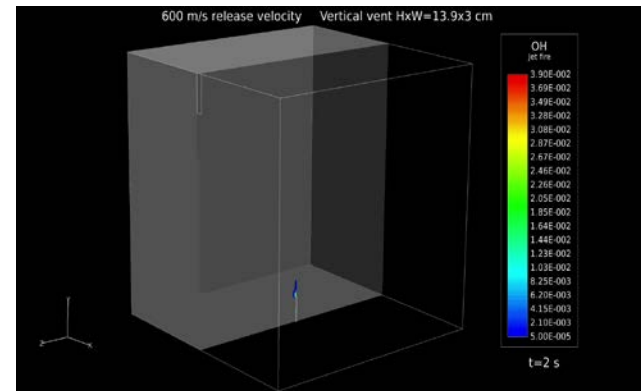
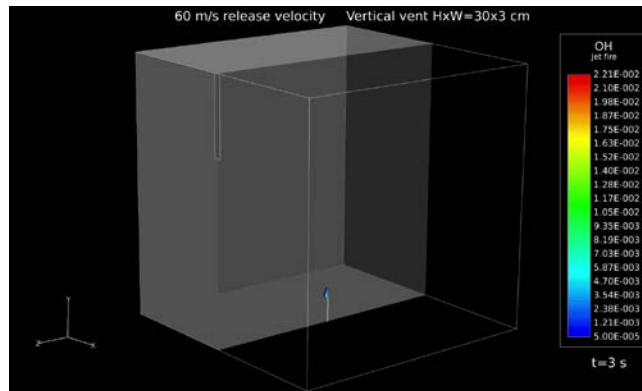
### Fire regime vs. flow rate

- ❖ Well ventilated fire (small leak rates)
- ❖ Under-ventilated fires
  - External flame (moderate flow rates)
  - Self-extinction (higher flow rates)
  - External flame (very high flow rate)

Need for detailed chemistry



EDC combustion model





# Progress: blast waves

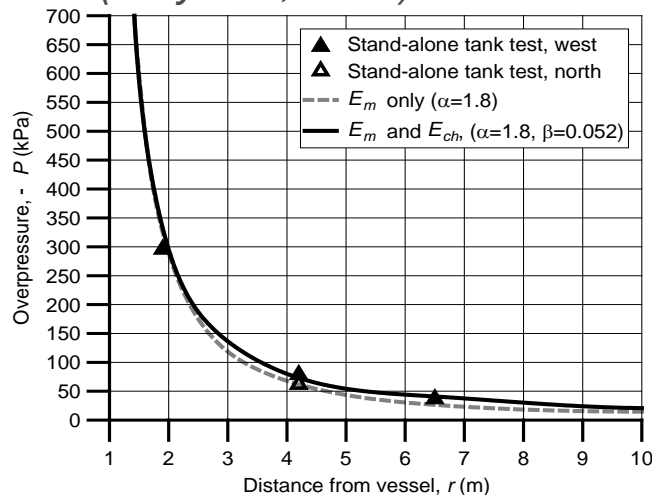
## Analytical blast wave decay model

- ❖ Real gas EOS
- ❖ Chemical energy ( $H_2$  combustion in air) added dynamically to hydrogen mechanical compression energy

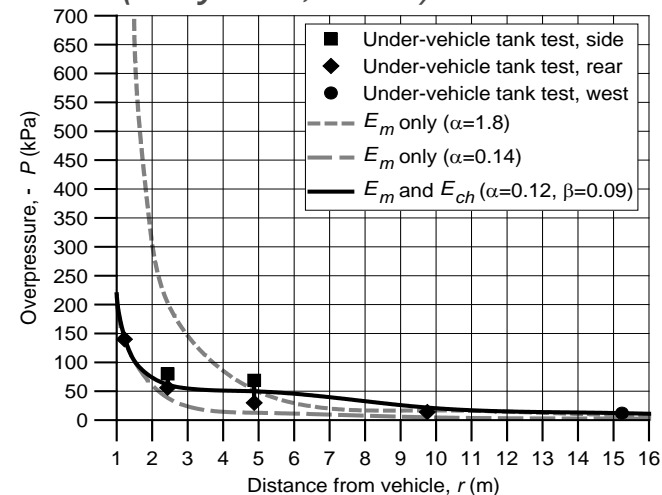
$$\Delta E_m = \frac{(p_g - p_s) \cdot (V - mb)}{\gamma - 1}$$

$$\bar{r}_P = r \left[ \frac{p_s}{\alpha \cdot E_m + \beta \cdot \left( \frac{r_{sh}}{r_b} \right)^3 \cdot E_{ch}} \right]^{1/3}$$

**Stand-alone tank rupture**  
(Weyandt, 2005) validation

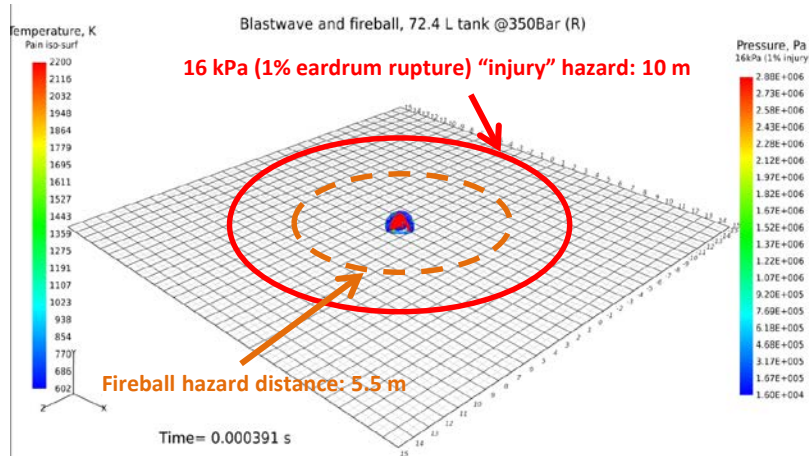


**Under-vehicle tank rupture**  
(Weyandt, 2006) validation



# Progress: blast waves

## CFD of blast wave and fireball radiation (ideal gas)



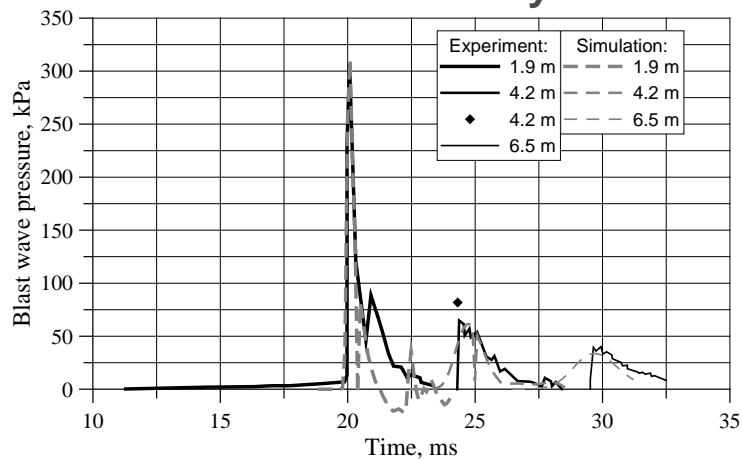
### Domain

- ❖ Blast wave hemisphere:  $R = 50$  m
- ❖ Fireball hemisphere:  $R = 10$  m
- ❖ Tank hemisphere:  $R = 2$  m
- ❖ Tank size  $L \times D = 0.66 \times 0.37$  m

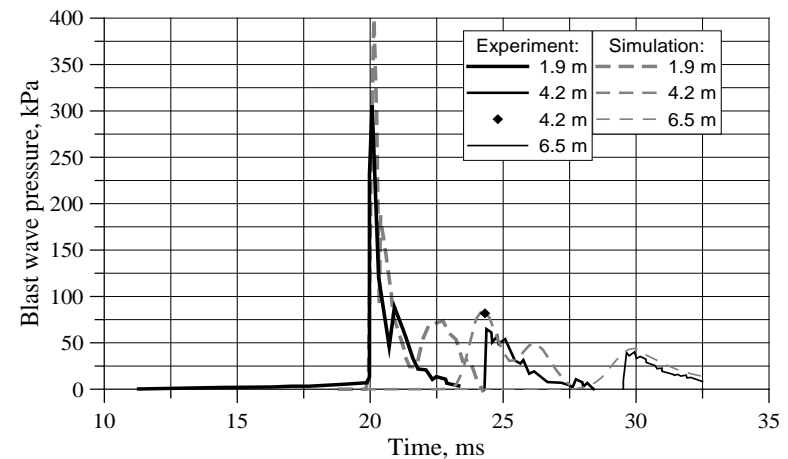
### CFD model

- ❖ RNG k- $\epsilon$  turbulence model
- ❖ EDC combustion model, 37-steps chemistry, ISAT algorithm
- ❖ DO radiation model

### Blast wave decay



- Overpressure transients (with radiation)

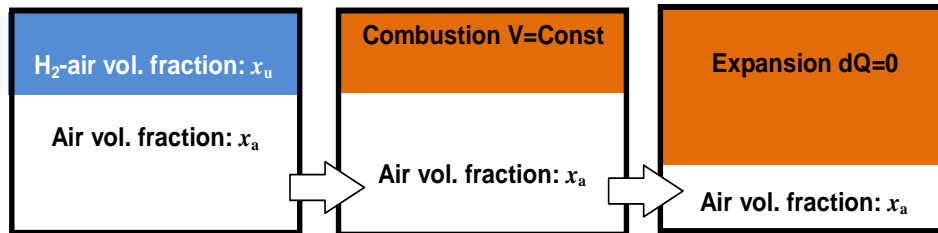


- Overpressure transients (no radiation)

# Progress: deflagrations

## Localised mixture deflagration (1)

Analytical model for maximum hydrogen inventory in a sealed enclosure



Initial parameters	Combustion V=Const	Expansion dQ=0
Initial state: $T_0, p_0$ H <sub>2</sub> : $m_{H_2}$ H <sub>2</sub> -air mixture: $m_u, M_u, V_u$ Air: $m_a, M_a, V_{a0}$	Burnt mixture: $m_b, T_{b1}, p_{b1}$ Air: $m_a, M_a, T_0, p_0$	Burnt mixture: $m_b, T_{b2}, p_2$ Air: $m_a, M_a, T_{a2}, p_2$

Analytical thermodynamic model for closed vessel deflagration:

$$p_2 = x_u p_{b1} \left( \frac{p_2}{p_{b1}} \right)^{\frac{\gamma_b - 1}{\gamma_b}} + x_a p_0 \left( \frac{p_2}{p_0} \right)^{\frac{\gamma_a - 1}{\gamma_a}}$$

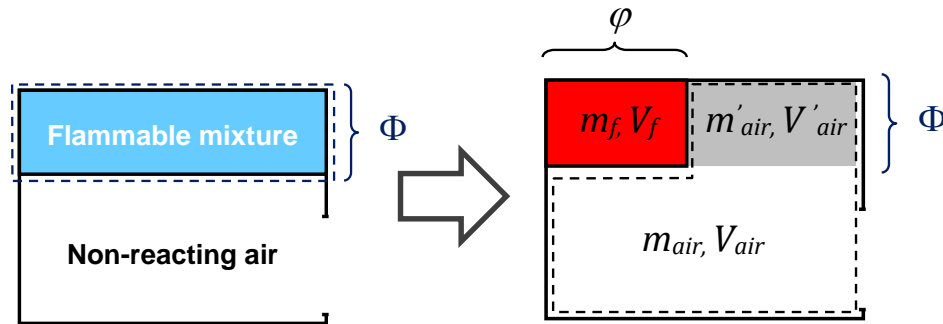
- ❖ Gives analytical expression for maximum overpressure in a closed space
- ❖ Validated against *Stamps D. et al., Proc. R. Soc. A, V.465, 2009*
- ❖ Allows to derive hydrogen inventory allowed to be released in closed space not to exceed a pressure threshold.
- ❖ For pressure threshold 10 kPa:

$$V_{H_2} (m^3) < 0.00314 \cdot V (m^3) \quad \text{or} \quad m_{H_2} (kg) < 2.61 \cdot 10^{-4} V (m^3)$$

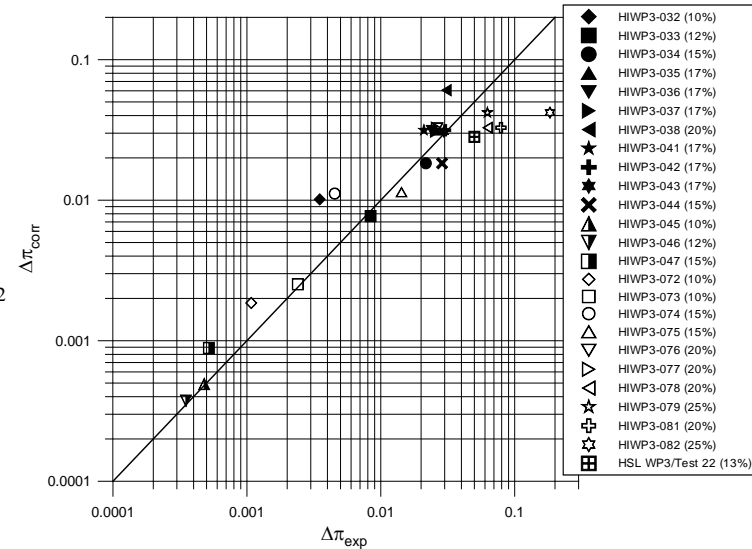
# Progress: deflagrations

## Localised mixture deflagration (2)

### Venting correlation for localised mixtures



$$\Delta\pi = 0.018 Br_t^{-0.92} \left[ \sqrt{\frac{E_i}{2}} \cdot MIN \left\{ 1.0; \left[ E_i^{2/3} \frac{1 + \left( \frac{1}{\phi} - 1 \right) \frac{M_{air}}{M_f}}{1 + \left( \frac{1}{\Phi\phi} - 1 \right) \frac{M_{air}}{M_f}} \right]^{2/3} \right\} \right]^2$$



- ❖ Applicable for vent sizing of low-strength equipment or buildings
- ❖ Only a small fraction of the non-uniform mixture with highest burning velocity (between 0.95 and 1.0 of  $S_u$ ) has decisive effect on the maximum overpressure
- ❖ Model validated against 25 uniform and non-uniform mixture experiments carried out in facilities at KIT (Germany) and at HSL (UK)

# Progress: deflagrations

## Rayleigh-Taylor instability model

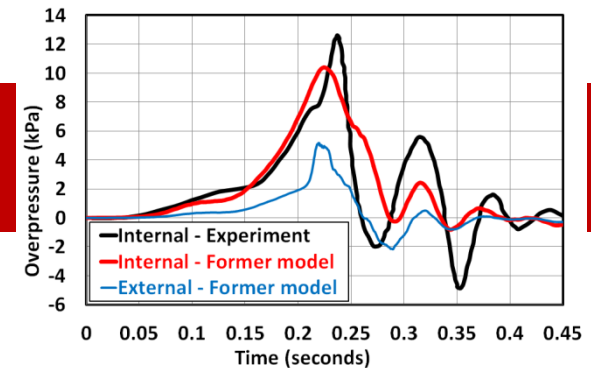
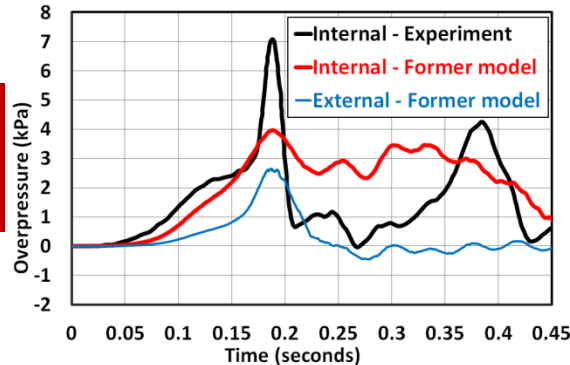
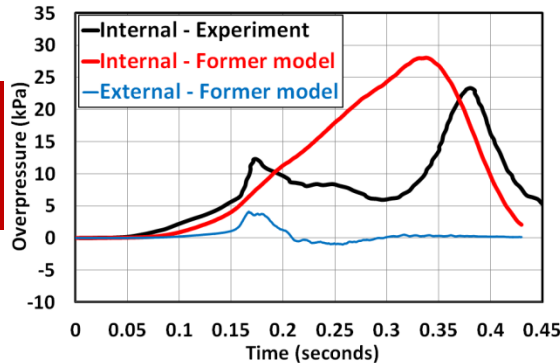
**Experiment:** C. Bauwens, J. Chaffee & S. Dorofeev, "Vented explosion overpressures from combustion of hydrogen and hydrocarbon mixtures," IJHE, vol.36, no. 3, pp. 2329-2336, Feb. 2011

Central ign. / 2.7m<sup>2</sup> vent

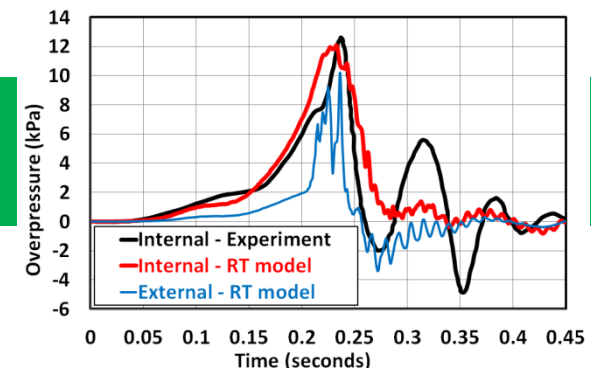
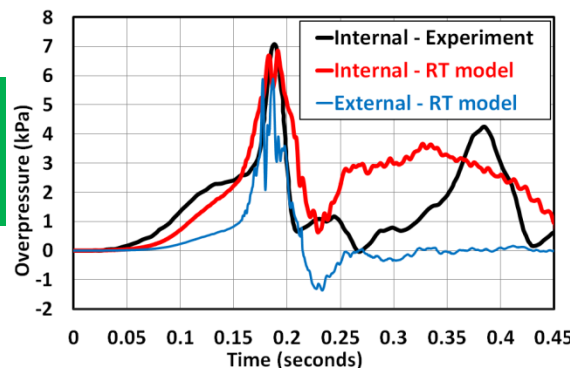
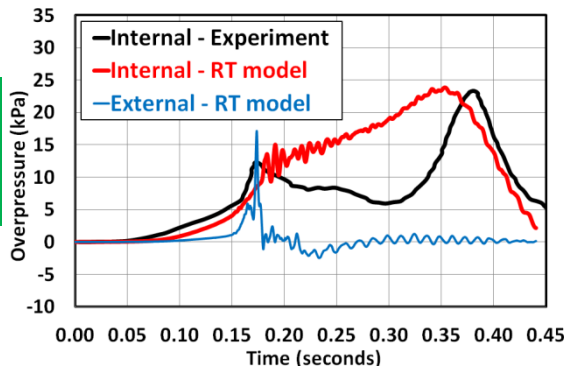
Central ign. / 5.4m<sup>2</sup> vent

Back wall ign. / 5.4m<sup>2</sup> vent

Former model results:

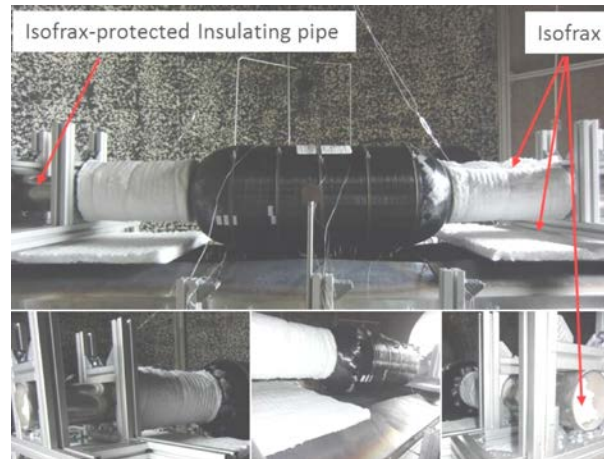


RT model results:



# Progress: storage safety

## Thermal protection and fire resistance



Exp. No	Tank condition	Tank condition	HRR, kW	Protection	Ambient gas	Filling gas	FRR
1	Bare	New	170	-	$N_2$	$H_2$	8 min
2	Bare	Used	170	-	$N_2$	$H_2$	9.7 min
3	Bare	Used	79	-	$N_2$	$H_2$	16 min
4	Protected	Used	170	Intumescent paint, 7 mm	Air	He	1 h 7 min
5	Protected	Used	170	Intumescent paint, 20 mm	Air	He	1 h 50 min
6	Protected	Used	170	Outer shell	Air	He	1 h 13 min

HRR vs FRR

FRR vs thermal protection

- ❖ KIT HyKA facility, premixed burner (Int. Access programme within H2FC project)
- ❖ Type 4, pressure loaded tanks, bare and protected, 6 completed fire tests
- ❖ Uncertainty in heat release rating (HRR) allows for discrepancy in fire resistance between test centres
- ❖ Achieved fire resistance rating (FRR) **1h 50min** - beyond the longest experimental car fire **1h 40min**

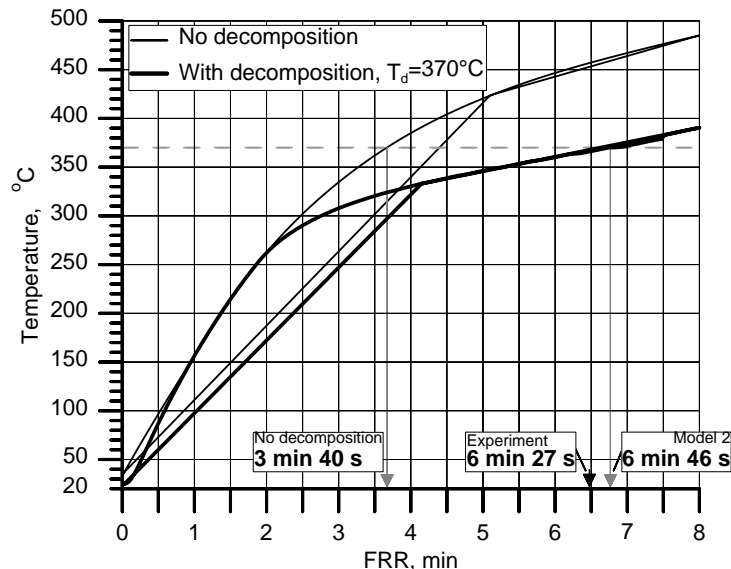
# Progress: storage safety

## Conjugate heat transfer to tank in fire

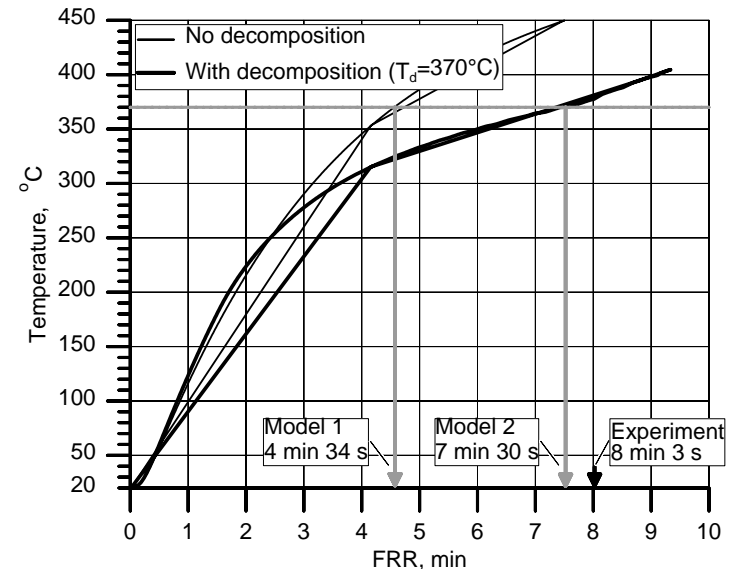
### CFD model to predict tank failure

- ❖ Segregated incompressible solver, SIMPLE algorithm
- ❖ Standard  $k - \varepsilon$  model with wall functions
- ❖ Eddy-Dissipation model
- ❖ Discrete Ordinates radiation model with WSGG
- ❖ Tank failure criterion based on decomposed wall thickness

**Non-premixed propane burner test**  
(Weyandt, 2005)



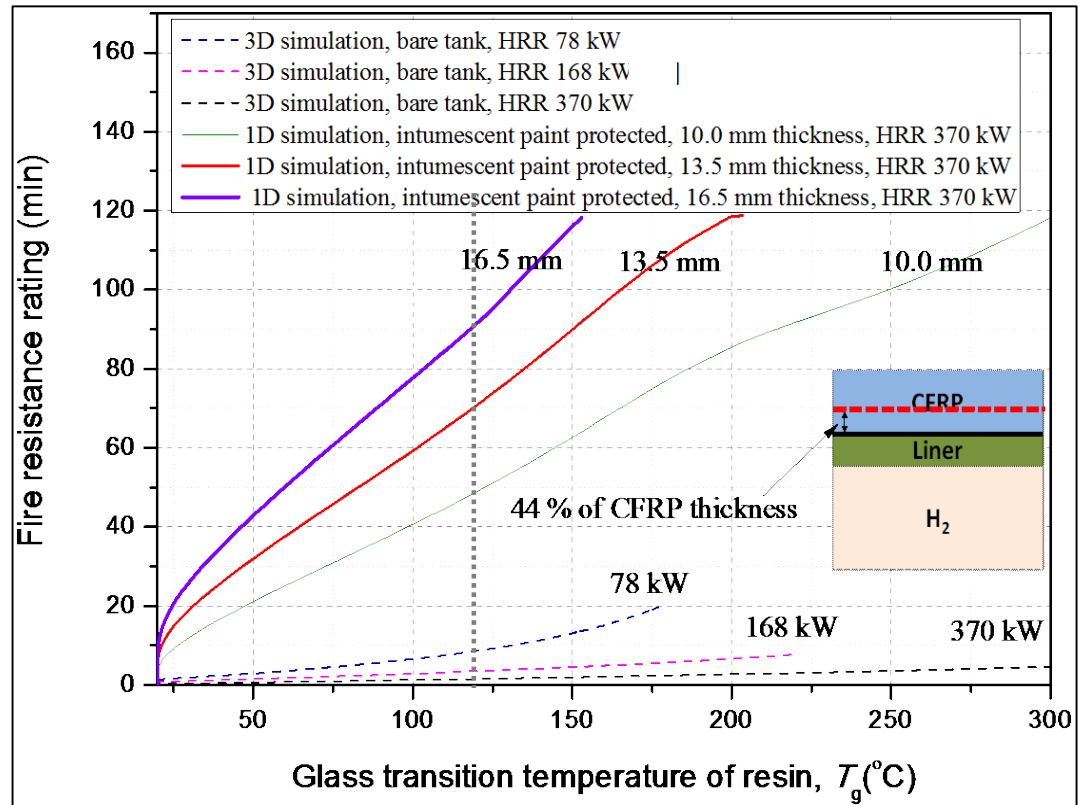
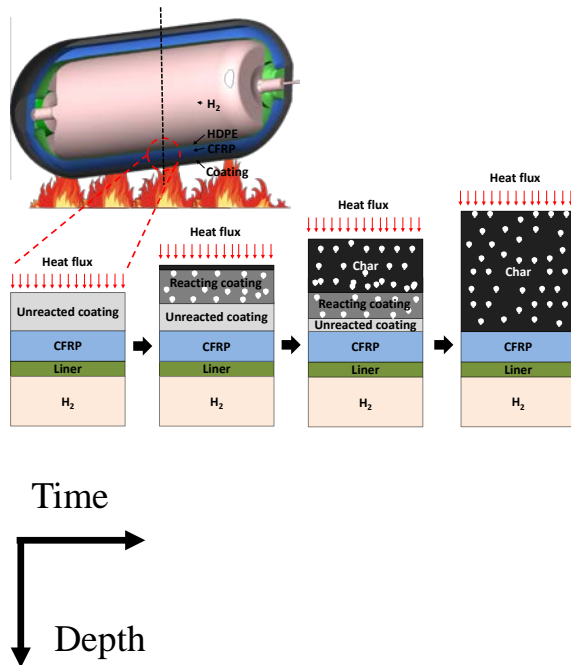
**Premixed burner test**  
(KIT facility)





# Progress: storage safety

## CFD study of intumescent paint protection



**Thermal protection can increase FRR by order of magnitude!**



# Working topics

## Releases and jet fires

- ❖ Transient solution for under-expanded jet fire lift-off and blow-off
- ❖ Delayed ignition of high-pressure releases
- ❖ CGH2 and LH2 jet fire flame length and radiation
- ❖ Effect of impinging and attached jets on hazard distances

## Blast waves and fireballs

- ❖ Blast wave and fireball dynamics from high-pressure tank rupture accounting real gas properties and effect of radiation effect on blast wave decay
- ❖ Thermal radiation from fireballs

## Deflagrations and detonations

- ❖ Non-uniform vented deflagration (further model validation)
- ❖ DDT modelling and simulations in large industrial scales

# Working topics

## Storage safety

- ❖ Breakthrough explosion-free (leak-no-burst) technology for CGH<sub>2</sub> storage in composite tanks (patent application GB1602069.5 Composite pressure vessel, 05.02.2016)
  - Following outcomes of the UK EPSRC H<sub>2</sub>FC SUPERGEN Hub and SUPERGEN Challenge projects
- ❖ Parametric study to underpin proposal for update of GTR#13 fire test protocol
  - Effect of HRR
  - Effect of burner design and type

# New directions

- ❖ Update of GTR#13 fire test protocol to harmonise test procedure and eliminate test results discrepancy in different laboratories:
  - Definition of representative value of heat release rate of test fire to reflect parameters of real car fires
  - Establish requirements to “standard” burner design
- ❖ Radiation heat transfer modelling and numerical simulations to characterise hazards related to high-pressure storage and components at refuelling stations.
- ❖ Breakthrough safety technologies development and validation, e.g. exclusion of catastrophic tank rupture in a fire.

# New directions

- Prevention and mitigation of blast wave in confined space such as tunnels, garages, car parks, HRS, etc.
- Time to rupture of high-pressure vessel, e.g. tube at road accident, subject to jet fire from high-pressure equipment, e.g. another tube.
- Efficiency of blast barrier designs.
- Harmful pressure and thermal effects on first responders (with protection).
- Pressure peaking phenomena for ignited releases.
- Thermal loads of indoor fires and effect of water condensation.
- Attached and impinging jets: CFD modelling and engineering correlations.
- LH2 tank rupture and rapid phase transition pressure loads.

# New directions

- Liquefied hydrogen release, dispersion and ventilation, including under wind conditions.
- Combustion of cold hydrogen jets and clouds during and after LH2 release.
- Passive ventilation for multiple vents under realistic wind conditions.
- Validation experiments for: under-vehicle tank rupture, tanks of different volume and pressure, etc.

**Thank you for your  
attention!**

